

# CO<sub>2</sub> ADSORPTION ON AMINE MODIFIED MESOPOROUS SILICAS: STUDY OF THE PROGRESSIVE DISORDER ON THE HONEYCOMB ARRANGEMENT.

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**RESUMO:** Neste trabalho, estudou-se a influência de alterações na estrutura porosa tipo “favo de mel” típica da classe de sílicas mesoporosas SBA-15 sobre a adsorção de CO<sub>2</sub>. SBA-15 foi sintetizada por via hidrotérmica (S00) e por outras rotas que introduziram modificações, como expandir o poro usando heptano (S10), reduzir o comprimento dos canais e modificar a estrutura hexagonal da sílica por adição de quantidades crescentes de fluoreto de amônio (S11, S12, S13 e S14). Todos estes materiais foram funcionalizados pela ancoragem de amino-propil trietoxissilano (APTES) à superfície da sílica ou por impregnação de polietilenoimina (PEI). As isotermas de CO<sub>2</sub> foram obtidas e matematicamente tratadas para todos os adsorventes usando o modelo de Langmuir de duplo sítio (“Dual Site”) e a influência da estrutura foi relacionada com as diferentes capacidades de CO<sub>2</sub>. Comprovou-se que a adição de fluoreto é importante na regulação da quantidade de CO<sub>2</sub> adsorvida por fisissorção e quimissorção.

**PALAVRAS-CHAVE:** APTES, quimissorção, fluoreto, SBA-15.

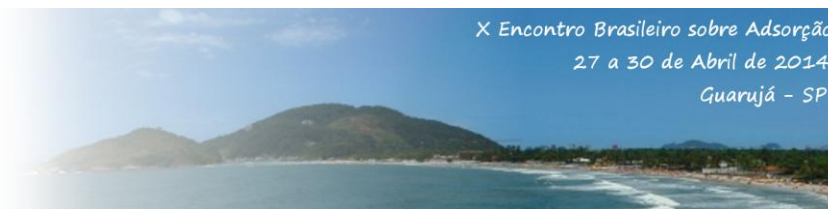
**ABSTRACT:** In this work, the influence of changes in the typical honeycomb structure of APTES grafted SBA-15 on the adsorption of CO<sub>2</sub> was studied. SBA-15 was synthesized hydrothermally (S00) and by introducing some modifications, such as pore expansion using heptane (S10) and changes in the hexagonal arrangement of the silica by adding increasing amounts of ammonium fluoride (S11, S12, S13 and S14). All of the synthesized silicas had either its surface grafted with 3-triethoxysilyl propylamine (APTES) or impregnated with polyethyleneimine (PEI). CO<sub>2</sub> isotherms were measured and well described by the Dual site Langmuir model for all adsorbents and CO<sub>2</sub> uptakes were correlated with the different frameworks. It was found that the addition of fluoride is a key factor in the regulation of CO<sub>2</sub> uptake by physisorption and chemisorption.

**KEYWORDS:** APTES, chemisorption, fluoride, SBA-15.

## 1. INTRODUCTION.

Global warming resulting from the emission of greenhouse gases has received widespread attention due to the significant and continuous rise in atmospheric CO<sub>2</sub> concentration, mainly by the extensive utilization of fossil fuels. Previous researchers have established that

anthropogenic CO<sub>2</sub> accounted for more than 60% of the total emissions leading to global warming (Houghton et al., 1990). Accordingly, considerable efforts have been devoted to develop new technologies to redress the massive CO<sub>2</sub> discharges. Generally, the main approaches to the separation of CO<sub>2</sub> are cryogenic distillation, membrane purification, absorption with liquids and



adsorption using solids (Choi et al., 2009; Douglas et al., 2005). The absorption with liquids is the most mature technology for large-scale CO<sub>2</sub> capture using aqueous alkylamine solutions or other fluids with basic character, such as chilled ammonia, which chemically absorbs the acid gases (Danckwerts, 1979; Astarita, 1961) However, the alkylamine solutions have some drawbacks such as high equipment corrosion rate due to evaporation process, high energy consumption in regeneration, loss of effectiveness over time due to low thermal stability and high footprint requirements (Rinker et al., 2000). An alternative technique to the sequestration of CO<sub>2</sub> is the adsorption over porous adsorbents functionalized with organic molecules containing amino groups due to its low energy requirement and easy operation and maintenance. In addition, the adsorption process exhibits several advantages over liquid amines such as a minor solvent loss that reduces the vessel corrosion and the regeneration process is easier (Sayari et al., 2011) Nevertheless, CO<sub>2</sub> adsorption in such materials is still far from the requirements of industrial practice so the optimization of the synthesis is a challenge for the researchers.

Several solid adsorbents may be suited for amine grafting, such as SBA-15 silicas (Wang and Yang, 2011) and mesocellular silica foams (Heydary-Gorji et al., 2011). These have received considerable research interest due to their high adsorption capacity, storage and selectivity towards CO<sub>2</sub>, SBA-15 being the most studied porous silica due to the larger pore size (5-30 nm) as well as a high wall thickness, which ensures its thermal, mechanical and chemical resistance in comparison with other hexagonal mesoporous silicas, as MCM-41.

## 2. EXPERIMENTAL.

### 2.1. Preparation of Siliceous Porous Structures.

Traditional SBA-15 was synthesized based on the method reported by Fulvio et al. (2005). Briefly, pluronic (P123) was firstly dissolved in 1.7 M HCl (aq.) at 313 K and then TEOS was added dropwise. The final molar composition of the synthesis gel was P123/SiO<sub>2</sub>/HCl/H<sub>2</sub>O = 0.018/1/6.364/202. The resulting suspension was stirred at 313 K for 24 h and then transferred to a Teflon-lined autoclave, where it was hydrothermally treated at 393 K for 72 h. The solid

was then filtered, washed with deionized water and dried at 333 K overnight (S00).

Mesocellular silica foams (MCFs) were prepared according to the water-alkane emulsion method proposed by Bao and co-workers (2006). In a first step, P123 and different amounts of NH<sub>4</sub>F were dissolved in 1.7 M HCl (aq.) at 313K for 24 h, and then TEOS was premixed with heptane and added into the transparent solution with further stirring for 24 h at room temperature. The final molar ratios in the synthesis gel were set to P123/SiO<sub>2</sub>/HCl/NH<sub>4</sub>F/heptane/H<sub>2</sub>O = 0.018/1/6.364/0-0.065/4.273/202. The resulting white suspension was then transferred to a Teflon-lined autoclave and hydrothermally treated at 393 K for 72 h. The solid was finally filtered, washed with deionized water and dried overnight at 333 K.

All materials were calcined from room temperature to 550 °C at a heating rate of 1 °C min<sup>-1</sup> and maintained at this temperature for 6 h. The mesostructured materials were denoted as S00 for the traditional SBA-15 and S1x ("1" for materials with heptane) where *x* increases from 1 to 4, standing for the F/Si molar ratio.

### 2.2. Grafting of 3-(triethoxysilyl)propylamine (APTES) and impregnation of poly (ethyleneimine) (PEI).

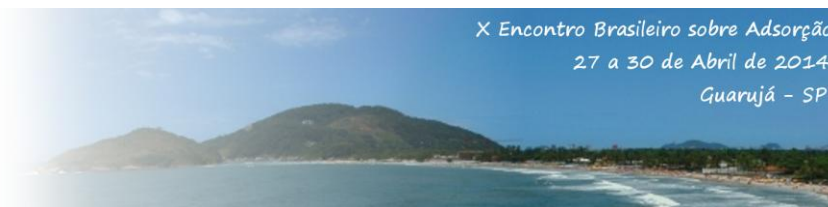
The grafting of APTES in each support was carried out by following the methodology reported by Hiyoshi et al. (2004). The impregnation via incipient wetness of siliceous porous materials was performed with PEI in methanol (Xu et al., 2003).

### 2.3. Characterization techniques.

The samples were characterized by N<sub>2</sub> adsorption/desorption isotherms, transmission electron microscopy (TEM), X-ray diffraction; FT-IR spectroscopy and elemental chemical analysis.

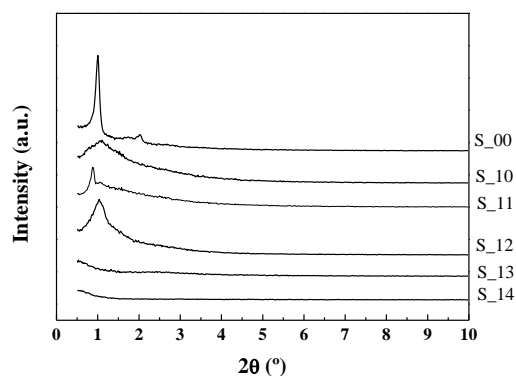
### 2.4. CO<sub>2</sub> adsorption tests

CO<sub>2</sub> adsorption isotherms were measured with a Micromeritics ASAP 2020 Analyzer (i.e., volumetrically) at 25 °C. Constant temperature circulating baths were used to maintain the sample at 25 °C. Prior to the measurements, samples were outgassed at 115 °C and 10<sup>-4</sup> mbar overnight



### 3. RESULTS AND DISCUSSION.

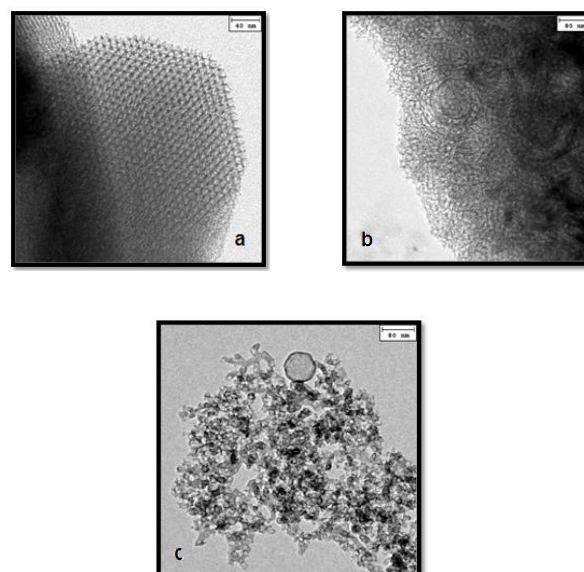
**3.1. Materials characterization:** Small-angle X-ray patterns of the synthesized porous silicas are shown in Figure 1. Conventional hydrothermal SBA-15 (S00) shows a typical XRD pattern of an ordered hexagonal network of mesopores with (100), (110) and (200) plane reflections that suggest a long-range order, characterizing a well-ordered mesoporous structure with P6mm hexagonal symmetry (Zhao et al., 1998) in some of the studied samples. TEM micrograph reveals a well-ordered honeycomb structure which agrees with the findings from the small-angle XRD diffractogram.



**Figure 1.** XRD patterns of pure SBA-15 (S00), SBA-15 with heptane (S10) and with heptane and rising the amount of fluoride (S11, S12, S13 and S14).

The addition of the swelling agent during the synthetic process, such as heptane, leads a poor resolution of the (100) diffraction peak and the absence of the (110) and (200) reflections, which suggests that pore swelling agents like heptane attach to the surface functional groups giving rise to less ordered materials. This disordering effect was confirmed by TEM micrographs (Figure 2).

With this respect, other authors (Schmidt-Winkel et al., 2000) have established that the transition from the hexagonally structured SBA-15 and a mesocellular foam takes place due to an increase in the pore size caused by such swelling agents as alkanes or benzene derivatives compounds, which penetrate into the hydrophobic core of the surfactant micelle, disrupting the typical honey comb packing of the hydrothermal SBA-15 by leading the nodes to separate into spherical micelles and aggregate to form the mesocellular foam material, as revealed by the TEM micrographs.



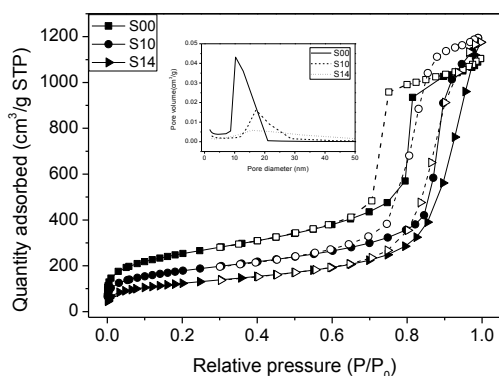
**Figure 2.** TEM micrographs of (a) SBA-15 (S00), (b) SBA-15 with heptane (S10) and (c) with the highest fluoride load (S14) and heptane.

In figure 3,  $N_2$  adsorption/desorption isotherms are shown for samples S00, S10 and S14. The addition of ammonium fluoride produces a shift of the hysteresis loop to higher relative pressure. Low loads of ammonium fluoride lead to a significant decrease in the surface area (Table 1). Nevertheless, for higher fluoride content, the surface area and nitrogen adsorbed at higher relative pressure increase with narrow hysteresis loop, which indicates the formation of a uniform structure with larger pore size. Textural properties (see Table 1.) suggests a progressive loss of the ordered framework leading to a structure with low porosity that evolves to MCF structure when the fluoride content is increased, in according with DRX patterns.

**Table 1.** Textural properties of pure mesoporous silicas

|     | S<br>(m <sup>2</sup> /g) | D <sub>p</sub><br>(nm) | V <sub>p</sub><br>(cm <sup>3</sup> /g) | V <sub>mpDR</sub><br>(cm <sup>3</sup> /g) |
|-----|--------------------------|------------------------|--|---|
| S00 | 908                      | 7.95                   | 1.70                                   | 0.45                                      |
| S10 | 643                      | 10.7                   | 1.84                                   | 0.32                                      |
| S11 | 392                      | 16.6                   | 1.03                                   | 0.24                                      |
| S12 | 542                      | 13.5                   | 1.71                                   | 0.28                                      |
| S13 | 418                      | 15.3                   | 1.68                                   | 0.15                                      |
| S14 | 447                      | 17.3                   | 2.33                                   | 0.23                                      |





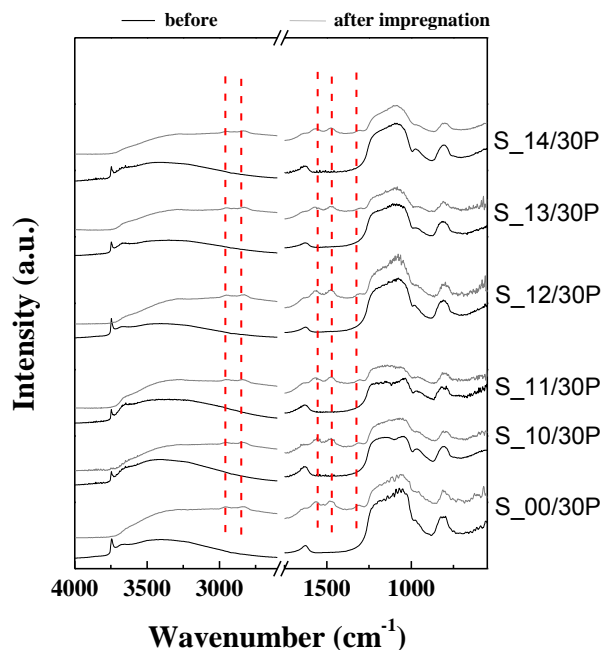
**Figure 3.** Nitrogen adsorption/desorption isotherms at  $-196^{\circ}\text{C}$  for pure supports S00, S10 and S14.

The vibration frequencies and their respective roles in the porous silica framework were examined by FT-IR spectroscopy in the range of  $4000\text{--}400\text{ cm}^{-1}$ . The FT-IR spectra for all samples are typically dominated by the Si–O–Si asymmetric stretching at  $1054\text{ cm}^{-1}$  with a shoulder at  $1160\text{ cm}^{-1}$ , revealing the existence of a dense silica network, where oxygen atoms play the role of bridges between two silicon sites. The symmetric vibration at  $805\text{ cm}^{-1}$  was assigned to the Si–O–Si bending mode. The band at  $960\text{ cm}^{-1}$  can be assigned to the Si–O in-plane stretching vibrations of the silanol Si–OH groups generated by the presence of defect sites (Colilla et al., 2010). The bands in the range of  $3740\text{--}3415\text{ cm}^{-1}$  were assigned to the overlapping of the O–H stretching bands of hydrogen-bonded water molecules (H–O–H) and Si–OH stretching mode of surface silanol hydrogen bonded to molecular water ( $\text{SiOH}\cdots\text{H}_2\text{O}$ ) (Gallas and Lavelley, 1990). Finally, the band located at  $1631\text{ cm}^{-1}$  has been assigned to H–O–H bending vibrations (Colilla et al., 2010).

The functionalization of silica porous materials with organic molecules containing amino groups reveals the presence of two bands located at  $2950$  and  $2840\text{ cm}^{-1}$  assigned to C–H asymmetric stretching and symmetric stretching modes of PEI (Figure 3) and APTES chains (Drage et al., 2008). The bands centered between  $1565$  and  $1485\text{ cm}^{-1}$  are assigned to asymmetric and symmetric bending of primary amines ( $-\text{NH}_2$ ) (Wang et al., 2009). Nonetheless, the band located at  $1485\text{ cm}^{-1}$  can also be ascribed to the deformation of C–H bond (Lakard et al., 2004). The band located at  $1310\text{ cm}^{-1}$  has been assigned to NCOO- skeletal vibration

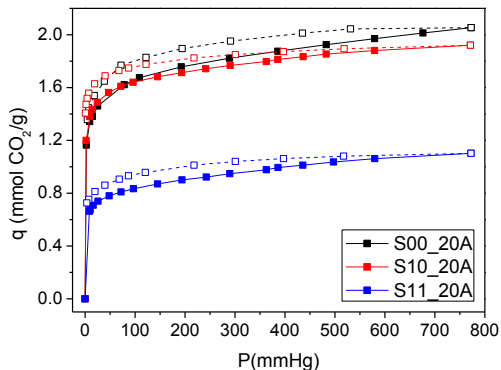
(Wang et al., 2009). Moreover, in the case of the grafted porous silica, the presence of two bands located at  $3364$  and  $3289\text{ cm}^{-1}$ , assigned to N–H stretching vibration, is noticeable (Wang et al., 2009) and so is the presence of a band located at about  $687\text{ cm}^{-1}$ . It has been ascribed to the presence of N–H bending vibrations, indicating that the amine group in APTES-functionalized SBA-15 material has been successfully obtained (Han et al., 2007). Finally, the intensity of the band corresponding to silanol groups ( $960\text{ cm}^{-1}$ ) decreases and/or is not observed in the FT-IR spectra of the functionalized porous silicas, suggesting a possible reaction between the silanol group from the silica surface and the amine group of PEI or APTES, giving evidence to the covalent bonding of organic molecules containing the amino group in porous silica materials.

### 30% PEI series

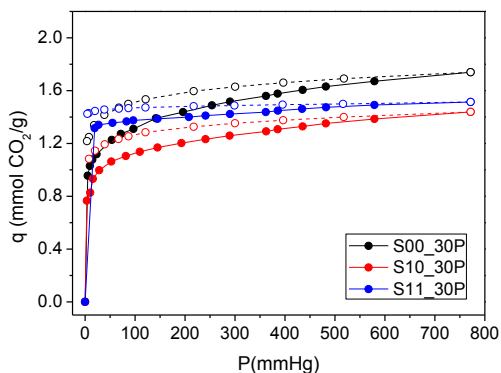


**Figure 4.** FTIR spectra of the pure supports (Black line) and after impregnation with 30% PEI (grey line)

**3.1.  $\text{CO}_2$  adsorption isotherms** Some selected  $\text{CO}_2$  isotherms at  $25^{\circ}\text{C}$  for the grafted and impregnated series are shown in Figs. 5 and 6, respectively. The structure of all adsorbents and the chemistry of amino sources have an important influence in  $\text{CO}_2$  uptakes. In fact, the measured experimental data were well fitted by Dualsite Langmuir model (Equation 1).



**Figure 5.** CO<sub>2</sub> isotherms at 25°C on grafted silicas S00, S10 and S11 with 20% APTES.



**Figure 6.** CO<sub>2</sub> isotherms at 25°C on impregnated silicas S00, S10 and S11 with 30% PEI.

$$Q = \frac{Q_{max1} * K_1 * P}{1 + K_1 * P} + \frac{Q_{max2} * K_2 * P}{1 + K_2 * P} \quad \text{Equation 1}$$

With this model, we have assumed (Vilarrasa-Garcia et al., 2014) that there are two different adsorption sites which are related to chemisorption (depends to amino groups,  $q_{m1}$ ) and

physisorption (related to siliceous framework, site 2,  $q_{m2}$ ). Tables 2 and 3 summarize DL model parameters for APTES-grafted and PEI-impregnated supports, respectively. CO<sub>2</sub>/N ratio and % N (wt) as determined by elemental analysis are also showed.

If only the adsorbents prepared with fluoride were considered, it can be observed that the increase in the amount of fluoride promotes an increase in the physical affinity as reflected in the larger  $K_2$  obtained. However, the less ordered structure of these solids impedes the presence of two adjacent amino groups when APTES is grafted, which are required to react thus the addition of fluoride provokes a decrease in the availability of chemisorption sites.

In the case of the adsorbents impregnated with PEI, it can be observed that the ratio  $q_{chemisorption}/q_{total}$  increases with the addition of fluoride. The presence of PEI blocks micropores, which leads to a decrease in physisorbed CO<sub>2</sub>, especially in the samples with a larger microporosity. Although the PEI-impregnated adsorbents have inaccessible amino groups below 75°C, CO<sub>2</sub> capacities obtained at 25°C are noticeable. On the other hand, the maximum value reached at 1 bar and 25°C is 2.3 mmol CO<sub>2</sub>/g (253 mg/g PEI) at a PEI load to 40%.

With the Dualsite model parameters, the contribution of physisorption and chemisorption were plotted as separate isotherms for all samples (see Figs. 7-10), corresponding to each of the two terms of the summation of the DL model. In these figures, it can be observed that S11 sample has the lowest physisorption capacity and when it is impregnated with PEI, it reaches the highest CO<sub>2</sub> capacity by chemisorption. With the addition of a low amount of fluoride (S11), 90% of highest chemisorption capacity is achieved.

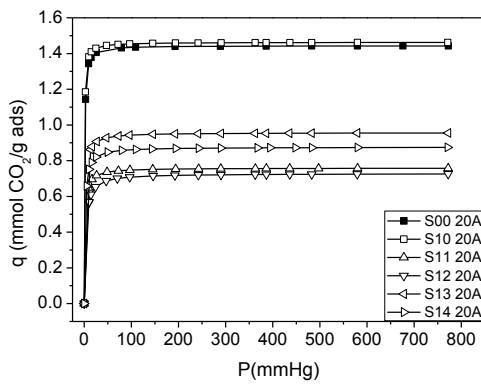
**Table 2.** DL model parameters and N content (% wt) obtained by chemical elemental analysis for grafted silicas

| 20 APTES | Q<br>(mmol CO <sub>2</sub> /g) | DualSite Langmuir |                |                   |                |        | %N   | mol CO <sub>2</sub> /mol N<br>chemisorption | %<br>q <sub>m1</sub> /q <sub>t</sub> |
|----------|--------------------------------|-------------------|----------------|-------------------|----------------|--------|------|---|--------------------------------------|
|          |                                | Q <sub>max1</sub> | K <sub>1</sub> | Q <sub>max2</sub> | K <sub>2</sub> | Chi2   |      |   |                                      |
| S14      | 1.33                           | 0.88              | 0.595          | 0.73              | 2.3E-3         | 3.2E-4 | 3.27 | 0.37  | 65.45                                |
| S13      | 1.37                           | 0.96              | 0.689          | 0.71              | 1.9E-3         | 8.6E-6 | 5.48 | 0.41  | 69.75                                |
| S12      | 1.18                           | 0.73              | 0.364          | 0.78              | 1.8E-3         | 1.6E-5 | 3.03 | 0.34  | 61.52                                |
| S11      | 1.11                           | 0.76              | 0.674          | 0.65              | 1.5E-3         | 1.5E-5 | 2.86 | 0.37  | 68.72                                |
| S10      | 1.92                           | 1.46              | 1.759          | 0.57              | 4.3E-3         | 2.1E-4 | 5.68 | 0.36  | 76.09                                |
| S00      | 2.12                           | 1.44              | 1.428          | 0.91              | 2.6E-3         | 7.3E-4 | 4.97 | 0.41  | 67.94                                |

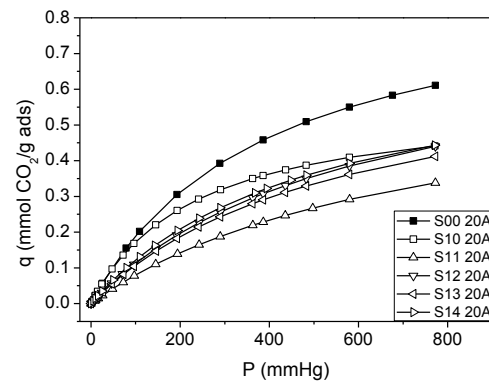
**Table 3.** DL model parameters and N content (% wt) obtained by chemical elemental analysis for impregnated silicas

| 30 PEI | Q<br>(mmol CO <sub>2</sub> /g) | DualSite Langmur  |                |                   |                |        | %N    | mol CO <sub>2</sub> /mol N<br>chemisorption | % q <sub>m1</sub> /q <sub>t</sub> |
|--------|--------------------------------|-------------------|----------------|-------------------|----------------|--------|-------|---|-----------------------------------|
|        |                                | Q <sub>max1</sub> | K <sub>1</sub> | Q <sub>max2</sub> | K <sub>2</sub> | Chi2   |       |   |                                   |
| S14    | 1.49(218) <sup>a</sup>         | 1.14              | 1.358          | 0.46              | 3.7E-3         | 8.2E-5 | 8.43  | 0.19  | 76.44                             |
| S13    | 1.34(196) <sup>a</sup>         | 1.11              | 2.589          | 0.35              | 2.5E-3         | 5.7E-5 | 7.21  | 0.19  | 82.41                             |
| S12    | 1.35(198) <sup>a</sup>         | 1.02              | 0.652          | 0.75              | 1.0E-3         | 2.3E-5 | 7.95  | 0.14  | 75.54                             |
| S11    | 1.51(221) <sup>a</sup>         | 1.35              | 1.933          | 0.61              | 5.0E-4         | 2.2E-5 | 10.24 | 0.24  | 89.19                             |
| S10    | 1.44(211) <sup>a</sup>         | 0.97              | 0.813          | 0.63              | 3.0E-3         | 4.9E-4 | 8.37  | 0.19  | 67.58                             |
| S00    | 1.74(255) <sup>a</sup>         | 1.13              | 0.891          | 0.86              | 2.9E-3         | 8.2E-5 | 8.53  | 0.19  | 64.72                             |

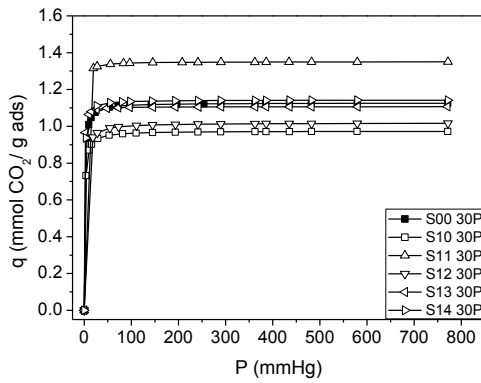
<sup>a</sup>CO<sub>2</sub> capacity in mg CO<sub>2</sub>/g PEI



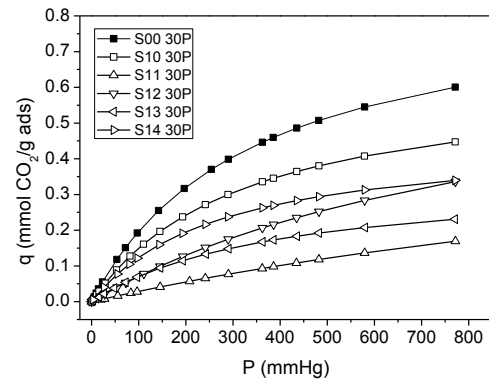
**Figure 7.** CO<sub>2</sub> chemisorption isotherms at 25°C obtained from DL model for all grafted silicas.



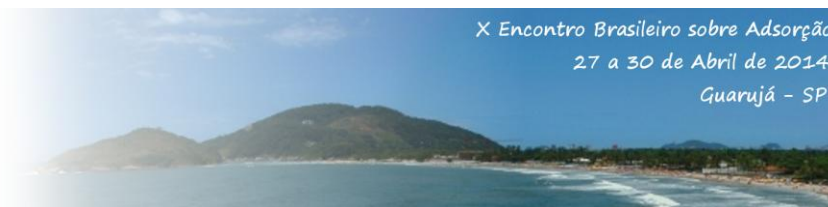
**Figure 8.** CO<sub>2</sub> physisorption isotherms at 25°C obtained from DL model for all grafted silicas.



**Figure 9.** CO<sub>2</sub> chemisorption isotherms at 25°C obtained from DL model for all impregnated silicas.



**Figure 10.** CO<sub>2</sub> physisorption isotherms at 25°C obtained from DL model for all impregnated silicas.



## 4. CONCLUSIONS

Several mesoporous silicas with a less ordered hexagonal structure have been synthesized. The evolution to less ordered materials was achieved by the addition of a swelling agent and modifying with the addition of different amounts of fluoride. The supports were loaded with amino groups by using two different strategies: PEI impregnation and APTES grafting. PEI and APTES, as amino sources, were effectively incorporated on the surface of materials, as confirmed by chemical elemental analysis and FTIR. Adsorbents who have a less ordered structure exhibit a better ratio chemisorption/physisorption and potentially these materials are interesting CO<sub>2</sub> adsorbents when the temperature is increased. The addition of low amounts the fluoride leads to hybrid material between honeycomb and MFC structure, decreases micropore volume and enhances the chemisorption ratio as it was reported in previous studies (Vilarrasa-Garcia et al., 2014).

## 5. ACKNOWLEDGMENTS

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